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COMBUSTION ANALYSIS OF AN OFF-ROAD SPARK IGNITION GASEOUS FUEL ENGINE

Allan Yao

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COMBUSTION ANALYSIS OF AN OFF-ROAD SPARK IGNITION GASEOUS FUEL ENGINE

Allan Yao

Thesis submitted to the Benjamin M. Statler College of Engineering and Mineral Resources at West Virginia University in partial fulfillment of the requirements for the degree of

Master of Science in Mechanical Engineering

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Keywords: Spark Ignition Engine, Natural Gas, Heat Transfer, Woschni Equation

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Abstract

COMBUSTION ANALYSIS OF AN OFF-ROAD SPARK IGNITION GASEOUS FUEL ENGINE

Allan Yao

The accurate calculation of the heat loss from bulk gas to engine coolant is critical for the optimization of the engine cooling system, calculation of the heat release rate, and improvement of the engine efficiency. The heat transfer coefficient of the traditional diesel and gasoline engines has been well documented. However, the research specific for the heat loss of spark ignition (SI) engine operating on gaseous fuels is limited.

This research developed a revised Woschni equation scaling factor for a Weichai turbocharged SI WP-10 engine operated on gaseous fuels. The engine was a 6 cylinder, 9.7 Liter stoichiometric engine developed to operate on gaseous fuels. The specific heat ratio was derived by calculating the specific heat of bulk gas which was a function of bulk gas mixture composition, and temperature. The scaling factors of the heat transfer coefficient was developed based on the hypothesis that the heat release rate was zero prior to the beginning and after the completion of combustion. When operated at full load, the scaling factors of the heat transfer coefficient for this engine was 0.34, 0.33, and 0.32 when operated on natural gas, natural gas & carbon dioxide, and natural gas & propane, respectively. Utilizing the revised Woschni equation, the heat release rate was calculated for each fuel. The effect of fuel composition and spark timing on cylinder pressure, heat release rate, mass fraction burned, combustion duration, and heat loss was analyzed. As expected, the blending of carbon dioxide to natural gas elongated the ignition delay, retarded the combustion phasing, and elongated the combustion duration. In comparison, the blending of propane accelerated the combustion process as indicated by the shorter combustion duration and ignition delay, and also the increased peak cylinder pressure. The effect of the fuel composition on the exhaust emissions before and after the three-way catalyst was also examined and presented.
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LIST OF SYMBOLS

A Heat transfer surface area
A_p Piston area
c_p Specific heat capacity under constant pressure
c_v Specific heat capacity under constant volume
D Cylinder bore
h Heat transfer coefficient
H_p Enthalpy of products
H_r Enthalpy of reactants
m_{air} Air mass per cycle
m_{CO_2} CO_2 mass per cycle
m_{final \ species} Final mass of species
m_{fuel2} Intake mass of fuel per cycle
m_{fuel3} Intake mass of fuel #2 per cycle
m_{intake} Intake mass per cycle
m_{intake \ addition} Added intake mass per cycle excluding fuel
m_{initial \ species} Initial mass of species
m_{fuel1} Intake mass of fuel per hour
m_{fresh} Fresh mass per cycle
m_{residual} Residual mass per cycle
m_{species,initial} Initial species mass
$M_{\text{species}}$ Molecular weight of species

$n_{\text{cylinders}}$ # of cylinders

$p$ Instantaneous pressure in cylinder (kPa)

$p_0$ Motoring pressure (only compression) (kPa)

$p_r$ Reference state of pressure (kPa)

$p_{\text{BDC}}$ Pressure at BDC

$p_{\text{calc}}$ Calculated pressure

$Q$ Heat transfer (kJ)

$R_{\text{mixture}}$ Gas constant of the mixture

$R_u$ Universal gas constant

$T_{\text{exhaust}}$ Exhaust temperature

$T_g$ Instantaneous temperature in the cylinder (Kelvin)

$T_{\text{initial}}$ Initial temperature in the cylinder

$T_n$ Temperature at next crank angle

$T_{n-1}$ Temperature at previous crank angle

$T_r$ Reference state temperature (Kelvin)

$T_W$ Chamber surface temperature (Kelvin)

$U$ Average gas velocity $\left( \frac{\text{m}}{\text{s}} \right)$

$V$ Cylinder volume (m$^3$)

$v_{\text{engine}}$ Engine Speed (RPM)

$\forall_d$ Total cylinder volume (m$^3$)
$V_{\text{min}}$ Minimum cylinder volume

$V_0$ Initial cylinder volume (m$^3$)

$V_p$ Piston cylinder speed (m/s)

$V_r$ Reference state cylinder volume (m$^3$)

$W$ Work produced at each crank angle

$\gamma$ Specific heat ratio

$\alpha$ Scaling factor

%MF$_{\text{fresh}}$ Percentage of mass fraction of fresh mixture

%MF$_{\text{residual}}$ Percentage of mass fraction of residual mixture

% MF$_{\text{final}}$ Percentage of mass fraction of final mixture
LIST OF ABBREVIATIONS

BDC Bottom dead center

BSFC: Brake specific fuel consumption

BSME: Brake specific mean emission

BTDC: Bottom dead center

BTE: Brake thermal efficiency

BTU: British Thermal Unit

CA Crank angle

CO Carbon monoxide

CO₂ Carbon dioxide

CHP Combined heat and power

CNG Compressed Natural Gas

DOE Department of Energy

EGR Exhaust Gas Recirculation

EIA Energy Information Administration

EPA Environmental Protection Agency

GC Gas chromatography

GDI Gasoline direct injection

HC Hydrocarbon

HD Heavy duty

HFID Heated flame ionization detector

HHV Higher heating value
HRR Heat release rate
ICE Internal Combustion Engine
LA Los Angeles
LD Light duty
MFB Mass fraction burned
mmBTU Million british thermal unit
NDIR Non-dispersive infrared
NGV Natural Gas Vehicles
NIST National Institute of Standards and Technology
NOx Nitrogen oxides
NMHC Non-methane hydrocarbon
OSC Oxygen storage capacity
Pd Palladium
RDE Real Driving Emissions
SI Spark Ignition
ST Spark timing
THC total hydrocarbon
TWC Three-way catalyst
US United States
Chapter 1 Introduction

Energy consumption throughout the world has continued to increase at an unrelenting pace. As the population from every part of the world is being lifted off of property, the demand for energy will continue to increase in the future to quench the world’s thirst for energy. Over the last century, the majority of energy was generated from one type of environmentally destructive type of fossil fuel: coal. However, the advancements in hydraulic fracturing, horizontal drilling, real-time logging analytics and programmable drill-heads allowed the United States to tap an energy resource: shale, which was not economically feasible before the 21st century. Furthermore, for the first time in decades, the Energy Information Administration (EIA) estimates that the United States (US) will become a net exporter of energy instead of a net importer, which is projected to happen in just 4 more years [1]. In addition, based on the current advancement of technology as of year 2018, natural gas (NG) will account for nearly 40% of United States total energy production by 2050 [1]. One of the major factors for the rapid increase in adoption of NG originates from it being one of the cleanest hydrocarbon fuels in the world. It has a low carbon footprint while the byproducts after combustion is significantly cleaner than gasoline or diesel. For instance, the major byproducts of NG combustion are carbon dioxide (CO₂) and water vapor. Furthermore, the emissions of nitrous oxides (NOx), hydrocarbon (HC), carbon monoxide (CO) and particulate matter (PM) from NG engines are significantly lower than emissions from diesel engines. With the low prices of NG in the United States, it has now become a fuel with comparable performance relative to its economics to justify consideration for widespread adoption. For reference, the cost of NG in US is $3 per million
British Thermal Unit (mmBTU), meanwhile Europe’s average price is $6/mmBTU and Japan’s average price is $8/mmBTU [2]. Furthermore, while the price of crude oil has risen by almost 50% in the past 2 years, the price of NG has just risen 5% [3]. In essence, the United States is positioned as one of the major world energy exporters in the coming decade.

NG has already been in use for vehicles throughout the United States, ranging from forklifts to transit buses. In addition, NG blends have also been utilized in the different types of engines. For instance, NG has high emissions of unburned hydrocarbons, which will become a factor in future emissions regulations. Therefore, CO₂ has been utilized in NG blends on NG spark ignition (SI) engines, which will increase the engine brake specific fuel consumption (BFSC) by almost 5% due to the lower heating value of the fuel blend, but yield a reduction of 80% in NOx emissions [4]. The drastic decrease in NOx emission was mainly attributed to the lower combustion temperature. The CO₂ would act as diluents similar to a diesel engine’s exhaust gas recirculation (EGR) system. Furthermore, other blends, such as propane has been shown to demonstrate promise in improving the brake power of the engine, while lowering emissions as shown in a research done on SI engines in Turkey [5]. Currently, a substantial amount of NG engines in production utilize a SI system. The major factor for this situation as a result of the slower flame propagation rate of NG, subsequently resulting in increasing complications for ignition. Therefore, the SI NG engines are currently the most common NG engines found in the field. Hence, combustion modelling is extensive for SI engines, which would have defined most of the base models for simulations of heat transfer and combustion parameters. However, most of the
combustion models have been situated for engines operating on gasoline and diesel. One of the most renowned heat transfer correlation is the Woschni correlation, which is an experimental correlation that relates the different parameters of the engine resulting in an accurate heat transfer coefficient for the combustion gases inside the cylinder during operation. The significance of the correlation was to allow engineers and researchers to simulate the gross heat transfer that occurs during operation, which would be crucial for determining the engine efficiency and energy balance. For my research, the objective was to analyze the combustion processes of a SI engine operated on different gaseous fuel mixtures. In addition, the heat loss would be calculated using experimental data from the field to iterate specific constants and scaling factor for a revised Woschni model for the different fuel mixtures that was tested. The conclusions about the significance of different fuel mixtures will be assessed to determine future feasibility of global adoption. In addition, exhaust emissions will be evaluated and compared to emissions regulations to determine current and future economic feasibility of NG engines. Finally, a small engine test cell was designed and set-up for a direct comparison between NG and gasoline.
Chapter 2 Literature Review

Gaseous Fuels

Advancements in fossil fuel extraction technology fueled the growth in NG and crude oil production in the US. Eventually, the excess supply lead to a deterioration in the worldwide prices of crude oil and NG due to a supply glut. From October 2014 to January 2016, the price of crude oil crashed over 55% [6], while the price of NG tumbled 30% [7]. Nonetheless, NG and crude oil worldwide production is expected to rise about 10% in 2018 [8]. In consequence, fossil fuel consumption has also been steadily rising due to population growth and lower fuel prices throughout the world. Over the last 15 years, EIA has calculated that the energy consumption across the globe has grown by over 40% [8]. Moreover, gasoline and diesel hold over 80% of the market share for fuels utilized in transportation, while NG holds just 3% [9]. Currently, gasoline is utilized by 55% of every vehicle in the United States [9]. The characteristics of gasoline, such as high volatility, low expense and relative abundance have helped it become and remain the indisputable fuel of choice for transportation. However, there are significant CO₂ emissions, which is becoming more stringently regulated in the 21st century. Diesel is the second most utilized fuel utilized in transportation, but especially dominates in the heavy duty industry. The main factor is diesel engines on average tend to be more efficient than their gasoline counterparts. However, diesel engines tend to be larger is due to the existence of a more complex aftertreatment system designed to reduce the PM and NOx emissions. NG is another type of fuel that is utilized for transportation, which is slowly gaining market share. The reason is that due to the relative abundance of NG with the recent NG reserve discoveries, the prices have decreased substantially, leading to the economic feasibility of
widespread adoption. Unlike diesel and gasoline, NG have much lower emissions and a simple three-way catalyst (TWC) system can be applied to NG engines to yield regulatory complaint engines for production. However, in electricity generation, NG has become the dominant fuel source with a 32% market share in the US [10]. One of the most common types of NG power plants is combined heat power. As a result, research in this field is essential to determine the efficiency and power output of future NG engines.

Natural Gas

Across the major developed countries around the world, the United States has arguably the most advanced pipeline system for fossil fuel transportation. One of the major advantages of NG is its emissions. For example, on full engine load, NG has been shown to emit 30% less CO₂ comparable to gasoline for minor setbacks in performance [11]. Furthermore, another advantage of NG is in its abundance throughout the world. It is estimated that 55% of the world’s current crude oil reserves are in regions of frequent political turmoil [12]. In 2016, United States produced about an average of 8.9 million barrels of oil per day, but US consumption was about 19.7 million barrels of oil per day [13]. The difference in production and consumption has been made up from imports of petroleum products, which is usually transported from the middle east. Unlike crude oil, where most of the resources presides in the volatile regions of the middle east, NG can be found in reservoirs throughout the world. Therefore, it is unlikely that a fuel shortage will occur due to supply or geopolitics, such as the 1973 oil crisis, since a monopoly over the NG supply is unfeasible. In the US, the EIA currently estimates there are proven NG reserves of over 324 trillion cubic feet in 2016, which has risen by 5% from 2015 [14]. Based on current US
consumption rate, the NG supplies will last for over a century. Furthermore, the NG has already been proven to work in developing countries such as Brazil and Argentina, where over 1.5 million vehicles run on solely compressed natural gas (CNG) for propulsion [15]. As a result, the United States would definitely utilize NG during the transition between fossil fuels to green energy in the coming decades.

NG is one of the most established alternative fuels currently on the market. As shown in the Table 2-1 [16], NG is mainly composed of methane (CH$_4$) in addition to some heavier hydrocarbons. As a result, NG is usually approximated based on its CH$_4$ qualities. If computational power is adequate, model simulations might include traces of ethane and propane, but the gases that are ranging from trace amounts to less than one percent are not generally considered in the simulation models due to computational limitations.

Table 2-1: Typical Chemical Composition of Natural Gas in the United States

<table>
<thead>
<tr>
<th>Component</th>
<th>% Mole Analysis</th>
<th>Range (% mole)</th>
</tr>
</thead>
<tbody>
<tr>
<td>Methane</td>
<td>93.9</td>
<td>87.0 - 97.0</td>
</tr>
<tr>
<td>Ethane</td>
<td>4.2</td>
<td>1.5 - 9.0</td>
</tr>
<tr>
<td>Propane</td>
<td>0.3</td>
<td>0.1 - 1.5</td>
</tr>
<tr>
<td>iso - Butane</td>
<td>0.03</td>
<td>0.01 - 0.3</td>
</tr>
<tr>
<td>normal - Butane</td>
<td>0.03</td>
<td>0.01 - 0.3</td>
</tr>
<tr>
<td>iso - Pentane</td>
<td>0.01</td>
<td>trace - 0.04</td>
</tr>
<tr>
<td>normal - Pentane</td>
<td>0.01</td>
<td>trace - 0.04</td>
</tr>
<tr>
<td>Hexanes plus</td>
<td>0.01</td>
<td>trace - 0.06</td>
</tr>
<tr>
<td>Nitrogen</td>
<td>1.0</td>
<td>0.2 - 5.5</td>
</tr>
<tr>
<td>Carbon Dioxide</td>
<td>0.5</td>
<td>0.05 - 1.0</td>
</tr>
<tr>
<td>Oxygen</td>
<td>0.01</td>
<td>trace - 0.1</td>
</tr>
<tr>
<td>Hydrogen</td>
<td>trace</td>
<td>trace - 0.02</td>
</tr>
</tbody>
</table>

**Natural Gas Engines**

Currently, in most modern vehicles NG is compressed in cylinders before it is utilized in vehicles, which is referred as CNG. The most common vehicles to use NG currently are
construction vehicles. The main reason is that construction vehicles are generally larger, which allows for larger compression NG tanks to be utilized. NGV’s, such as sedans on the road have significantly lower range due to the compact NG tank has to be fitted in the trunk or floor of the vehicle. Nonetheless, NG offers a myriad of significant advantages. NG has a higher octane number than gasoline, indicating a higher resistance to auto-ignition. Auto-ignition, also known as engine knock is extremely harmful for engines, since this phenomenon could destroy an engine in seconds. Auto-ignition arises due to flame detonation resulting from instantaneous combustion, leading to high pressure waves which can severely damage the engine piston, gasket, and other parts due to the loss of the boundary layer surrounding those engine parts. The reason is that the most common alloys utilized for engine piston construction is aluminum, which does not have a very high melting point. The boundary protects the cylinder from the heat, so manufacturers utilize aluminum because of its light weight and low cost. In essence, utilizing NG would help mitigate this problem by increasing the safety margin. In addition, this means that the fuel/air mixture are able to reach a significantly higher temperature and higher pressure before auto-ignition resulting in a higher energy output. This suggests that the compression ratio could be increased a higher amount on NGV than on gasoline vehicles. NG has higher low heating value than gasoline on mass basis, which means that it has a higher energy density. However, since NG is in gaseous form and gasoline is in liquid form, gasoline also have a higher net energy density. Higher compression ratios with the addition of NG are favored, but they might result in higher NOx emissions. Higher compression ratio results in lower knocking resistance, so it must be balanced. Lean combustion, which is the result of a
higher amount of air intake required for complete combustion of fuel in the mixture results in lower power output, but rich combustion, where higher fuel intake relative to the air intake results in HC and CO emissions. Research has illustrated that lean combustion of NG indicated slower flame propagation relative to gasoline [17]. For this reason, ignition for NG combustion is difficult to optimize for lean combustion. Another solution is EGR, which can be utilized to reduce knock occurrence. However, this reduces the amount of air circulating in the engine, resulting in lower volumetric efficiency. Furthermore, although EGR lowers NOx emissions, it leads to higher HC and CO emissions. As the EGR rate increases, the NOx emissions decrease almost linearly, while the HC emissions almost increases in line with EGR rate increases. As a result, there has been different NG mixtures currently being researched to lower the emissions while subsequently causing minimal effects to engine performance. From research done by a review on the effects of CO₂ and NG mixtures, the heating value of the fuel was decreased, which resulted in lower engine power output and thermal efficiency. The root cause of this efficiency decrease was the lower presence of NG and air due to the increased presence of CO₂ during stoichiometric combustion. From a study done on dual-fuel engines with CO₂ and NG mixtures, there was a 15-20% decrease in the power output due to volumetric efficiency decreases and slower flame propagation speed [4]. From the research, the carbon monoxide emissions were determined to be unaffected by the addition of CO₂. The NOx emissions reduction effects were similar to the EGR effects of the diesel engine combustion systems. A more complex gaseous mixture would include propane. Propane is one of the components of NG that has a higher lower heating value, lower auto-ignition temperature by almost 100 °C, and a
higher flame propagation rate. From research done by the DOE, it was determined that with the addition of propane, the same engine power output could be achieved with 5% of propane blended into the mixture in combination with a 5 -10% lower combustion temperature [18]. This lower temperature would decrease NOx emissions. Another advantage of NG engines is combustion noise compared to gasoline and diesel engines. NG has a slower flame speed than gasoline, so the combustion reaction is lower and generates less noise. Therefore, the compression ratio can be increased to optimize the efficiency of the engine, while generating similar noise comparable to a conventional gasoline engine.

From research done on NG engine models, the combustion noise can be further reduced by advancing ignition timing [19]. From research done between two modern light-duty passenger vehicles, the CNG vehicles exhibited a 3-9% lower fuel economy than the gasoline vehicle [20]. Even though the CNG engine was modified to increase its compression ratio, the increased flame speed of CNG caused efficiency reduction at medium engine loads. In the modern NG engines in production, several advancements in technologies have been implemented. Gasoline engine downsizing, which was made possible from turbocharging has trickled down into NG engines. In a research study done recently, a turbocharged CNG port fuel injection engine was compared to a gasoline version. From the comparison, the CNG engine lead to a 24.2% decrease in CO₂ emissions in addition to a 40% decrease in mileage costs [21]. From a recent analysis done on tractors, it was reported that significant fuel cost savings would be achieved if methane from agricultural waste was utilized instead of diesel fuels based on the market prices in
Although the tractor performance utilizing \( \text{CH}_4 \) was comparable to diesel, the fuel capacity was decreased. There is research being done on innovative NG engine technology such as thermochemical fuel reforming [23], but the current technology is not capable of calibrating a proper combustion methodology to optimize the method. However, optimizing emission reductions such as \( \text{CO}_2 \) has shown emission reductions of 25% [23], when applying current engine technology such as downsizing, EGR, increasing compression ratio and spark time advancing.

**Internal Combustion Engine Technology**

Internal combustion engine (ICE) has been recognized as one of the most popular power resource for its high thermal efficiency, reliability and durability. The research on ICE has focused on the improvement in thermal efficiency and the reduction in exhaust emissions. Among all factors affecting the engine thermal efficiency, the heat loss from the hot bulk gas in cylinder to coolant and lubrication oil has been recognized as the one having the most significant impact on engine efficiency [25]. Obtaining a better understanding of the heat transfer in ICE is crucial for the future optimization of ICE. The past research in this area has led to the development of numerous empirical equations calculating the heat loss of on-road diesel and gasoline engine. The latest development of the combined heat and power (CHP) system powered by stationary engine has initiated the interest of accurately estimating the heat loss from large stationary SI engines operated on NG. However, the research for heat loss from off-road SI NG engines has been limited.

Several key research areas are progressing in the ICE field. Several light duty (LD) gasoline concept engines are able to attain up to 18% reductions in emissions relative to
conventional engines in production by employing several key technologies such as gasoline direct injection (GDI) and turbocharging [26]. A turbocharger is just an additional component that utilizes the exhaust to generate power for a turbine used to power a compressor capable of boosting the pressure of the intake air. Meanwhile, heavy duty (HD) engines are able to achieve 50% brake thermal efficiency (BTE) utilizing techniques that are beginning to become commercialized such as complex EGR system and adaptive turbochargers [27]. Research currently indicates that utilizing a supercharger, a turbocharger, specially design piston bowl and complex aftertreatment could reach 55% BTE [28], which was demonstrated in the Cummins Super Truck [29]. Currently, HD industry achieves an industry average of about 40% [30]. Nonetheless, the HD NG engines have been increasing in market share. According to the American Public Association Transportation, one-third of all transit buses purchased in the United States in 2012 was CNG buses [31]. As iterated before, the fuel costs savings of switching to NG has been evident in the Lost Angeles (LA) metro buses, where there was a 10 – 20% reduction in operational costs for the NG buses compared to diesel buses [32].

**Aftertreatment & Three Way Catalyst**
Efficiency is one of the major focuses of the research and development (R&D) in the original equipment manufacturers (OEM’s), such as Toyota, Cummins, and Volkswagen. In the past decades, the efficiency and the reliability of engines have been continuously improved. According to the Pew Research Institute, the average MPG for automobile engines have doubled in the past three decades [33]. Meanwhile, emissions have decreased almost exponentially, with many modern vehicles emitting ten times less emissions than three
decades ago. Despite this, the emissions regulations throughout the world are projected to become increasingly stringent in the future. Europe is aiming to include the newly proposed Real Driving Emissions (RDE) particle number regulations, while China and India is aiming to achieve Euro 6 level regulations in the 2020 timeframe [34]. However, extensive improvements on RDE must be achieved before it is finalized. This is especially important in urban and congested areas, emissions from vehicles moving from idle to acceleration exhibit 10 times the emission limit [35], which are not included in the certification or RDE test cycles today. In addition, the regulations of the US Environmental Protection Agency (EPA) has also begun to become increasingly stringent with the possibility of the addition of a CO₂ emission standard [36].

The dominant after-treatment systems currently available are the TWC, diesel oxidation catalyst (DOC), diesel particulate filter (DPF), and selective catalytic reduction (SCR). Among these, TWC is the major after-treatment system for SI gasoline and NG engines. TWC is designed to remove harmful pollutants such as NOx, CO and HC from the exhaust. The nitrous oxides are converted to harmless nitrogen and carbon dioxide through chemical reactions from the solid catalyst, which is usually platinum or palladium (Pd). CO is reacted with oxygen resulting in carbon dioxide. Hydrocarbons are reacted with oxygen resulting in water and CO₂. In total, there is about fifteen simultaneous reactions occurring as the exhaust passes through the TWC. From a NG engine emissions study utilizing a Pd TWC, resulted in near 100% NOx and 80% CH₄ conversion rate [37]. In a laboratory reactor system composed of a TWC tested on a stoichiometric NG engine resulted in near 100% conversion rates for CO, NOx and CH₄ emissions [38]. In addition, Cummins recently achieved a breakthrough in oxygen storage capacity (OSC) model,
which was validated during TWC operation. Basically, this technology improved the efficiency of the TWC during operation by determining the temperature dependence of OSC model with the reductant [39].

**Heat Transfer Coefficient**

Calculating the accurate heat release rate (HRR) of an ICE is one of the most complex and challenging problems for all the OEM’s. To reiterate, the heat transfer coefficient remains one of the crucial pieces for solving the puzzle of calculating an accurate ICE efficiency. The heat transfer coefficient is a proportionality constant describing the relationship between the heat flux and thermodynamic forces. The main use of this proportionality constant is for calculating the heat transfer from bulk gas to coolant. Researchers utilize the heat transfer coefficient for calculating the heat loss from the engine cylinders over the entire working cycle, which would help improve the calculation of HRR. Despite this, an accurate theoretical approach for heat transfer does not exist. The available methods are composed of an array of theoretical and empirical correlations for heat transfer coefficient calculations. For example, Nusselt [40] was one of the first scientist studied the heat transfer in ICE. After analyzing experimental results, he managed to derive a general equation for the heat transfer coefficient for the cylinders in ICE:

\[
h = (5.388 \times 10^{-4}) \cdot (1 + 1.24 \cdot V_p) \cdot \frac{T_g^\frac{1}{3} \cdot p^\frac{2}{3} + 0.421 \cdot \left(\frac{T_g/100}{T_g-T_W}\right)^4 - \left(\frac{T_W/100}{T_g-T_W}\right)^4}{T_g - T_W}
\]  
Eq. (1)

\(T_g\) & \(p\) = temperature and pressure of working fluid/medium  
\(T_W\) = chamber surface temperature

Utilizing empirical data, Nusselt derived empirical correlations for heat transfer from volume, pressure and temperature.
However, Eichelberg [41] argued against the additive method that was proposed by Nusselt. Instead, he developed a novel method, which was deduced by the formula below:

$$ h = 77.9 \times 10^{-4} \cdot \left( \frac{T_g \cdot p}{V_p} \right)^{\frac{1}{2}} $$  \hspace{1cm} Eq. (2)

Rozenblit [42] used the assumptions of Belinsky [43] that there was radiation heat transfer in engines, to derive another heat transfer coefficient correlation:

$$ h = C_1 \cdot \left( \frac{C_u}{B} \right)^{\frac{1}{2}} \cdot \left( \lambda \cdot c_p \cdot \rho \right)^{\frac{1}{2}} \cdot \left( 1 + C_2 \cdot \frac{a \cdot W_{vs}}{c_u} \right) + \varepsilon \cdot \sigma \cdot \frac{T_p^4 - T_W^4}{T_p - T_W} $$  \hspace{1cm} Eq. (3)

$$ a = (k \cdot R \cdot T_g)^{\frac{1}{2}} - \text{acoustic speed,} \quad C_1 \text{ & } C_2: \text{empiric coefficients} $$

$$ W_{vs} = 2.43 \cdot \frac{n \cdot B \cdot \delta p}{k \cdot p \cdot \delta \phi} : \text{speed of vibrations} $$

$$ \text{Temperature permeability coefficient: } \zeta = (\lambda \cdot c_p \cdot \rho)^{1/2} $$

Finally, Woschni [43] developed a correlation for calculating the heat transfer coefficient which became widely used in engine research community. He assumed that the heat transfer was controlled by three factors: convection, radiation and rapid change in gas temperature. By assuming the heat transfer process is quasi-steady, the convection heat transfer coefficient can be calculated by equation:

$$ h = \alpha \cdot D^{m-1} \cdot T_g^{0.75 - 1.62m} \cdot p^m \cdot \left[ C_1 \cdot V_p + C_2 \cdot \frac{\forall_d \cdot T_r}{P_r \cdot V_r} \cdot (p - p_0) \right]^m $$  \hspace{1cm} Eq. (4)

m is the exponential factor given be the relationship: $\text{Nu} = C Re^m$

$$ \alpha: \text{scaling factor} $$

$$ p: \text{instantaneous pressure in cylinder} $$

$$ T_g: \text{instantaneous temperature in the cylinder} $$

$$ p_r, T_r, V_r: \text{reference states at beginning of combustion} $$
\( p_0 \): motoring pressure (assuming only compression)

By incorporating the piston speed in the equation, the Woschni equation took into account the swirling of the working medium during combustion. The reference states were taken before combustion takes place. The constants \( C_1 \) and \( C_2 \) were set as different values during different phases of the cycle. Therefore, Woschni took these processes into account by specifying specific expressions for calculating the constants at certain phases of the diesel engine cycle.

**Compression and Expansion:**

\[
U = 2.28U_{\text{piston}}, C_1 = 2.28, C_2 = 0 \quad \text{Eq. (5)}
\]

\[
U (\text{m/s})@\text{combustion} = 2.28U_p + 0.00324T_0 \frac{V}{V_o} \frac{\Delta P_c}{P_o}, C_1 = 2.28, C_2 = 3.24 \cdot 10^{-3} \quad \text{Eq. (6)}
\]

By applying the theory of similarity, Woschni accounted for the unsteady heat transfer occurring inside the combustion chamber. This was created by assuming that the flow in the cylinders were similar to the steady flow of a fluid in a pipe. Instead of a pipe, the fluid just flowed through the engine bore, while the average flow velocity was the average speed of the piston. The bulk gas was considered as a uniform working medium. For gasoline engines, the scaling constant was set to be 0.12793 by Woschni [44]. However, the research on NG engines indicates a higher scaling factor. Past research on determining the scaling factors vary for different engines. For diesel compression ignition engines, the scaling factors vary 0.73 based on HCCI engines [45]. For a 0.9 Liter four stroke SI gasoline engine, the scaling factor was calculated to be 0.82 [46], which was set in most SI models [47].
Chapter 3 Experimental Setup

The engine used was a Wechai, in-line 6-cylinder 9.7 Liter turbocharged SI stoichiometric gaseous fuel engine illustrated in Figure 3-1 below. This off-road engine was designed to operate with a stoichiometric air-fuel mixture. As shown in Table 3-1, the compression ratio was 9.7. The bore was 126 mm and stroke 130 mm. The fuel mixing and air/fuel ratio control system consists of the following system: (1) IMPCO control system including a variable venturi mixer; (2) Woodward fuel trim valve; (3) Woodward throttle Valve; (4) closed-loop control with Bosch LSU 4.9 wide band UEGO O₂ sensor for pre-catalyst O₂ measurement, and Bosch HEGO LSF 4.2 O₂ sensor for post-catalyst O₂ measurement. The premixed fuel entered before the turbocharger. The throttle valve was located upstream of the intake manifold. This engine was developed for off-road operation such as emergency power generation and water pump. All the experimental data was collected and provided by Wechai Power Ltd.

Figure 3-1: WP-10 SI NG Off-Road Engine
The test engine was coupled to a General Electric Dynamometer Model 42G408A and controlled by a Siemens SIMOREG CM 6RA70 designed to absorb the engine load and control engine speed. The in-cylinder pressure was acquired using a Kistler model 6125C11 pressure transducer at a 0.5° crank angle (CA) resolution. A digital data filter was applied to remove the noise of the pressure signal. At each operating point, the cylinder pressure of 200 consecutive cycles was measured, averaged, and processed to obtain the average cylinder pressure which was processed to derive the HRR, heat loss, and a set of combustion parameters. The exhaust gas was sampled for emissions measurement. In this research, the emissions of CO and CO$_2$ were measured using a non-dispersive infrared (NDIR) analyzer. The emissions of NO$_x$ were measured using a wet chemiluminescence analyzer. The emissions of total hydrocarbon (THC) were measured using a heated flame ionization detector (HFID). The emissions of CH$_4$ were measured using a HFID analyzer equipped with a non-methane cutter. The emissions of non-methane hydrocarbon (NMHC) was calculated by subtracting the CH$_4$ emissions from the THC emissions.

<table>
<thead>
<tr>
<th>Table 3-1: Engine Parameters</th>
</tr>
</thead>
<tbody>
<tr>
<td>Engine type</td>
</tr>
<tr>
<td>Engine speed</td>
</tr>
<tr>
<td>Compression ratio</td>
</tr>
<tr>
<td>Bore</td>
</tr>
<tr>
<td>Stroke</td>
</tr>
<tr>
<td>Length of Connecting Rod</td>
</tr>
<tr>
<td>Power</td>
</tr>
</tbody>
</table>

Table 3-2 presents the higher heating value (HHV) of three fuels examined in this research. The gas chromatograph (GC) analysis to NG reported a CH$_4$ number of 93.81, H/C ratio of 3.884, stoichiometric air/fuel ratio of 16.576. The NG blend Wobbe Index was 49.98. The first fuel was 100% NG. The second fuel mixture consisted of 73.4% NG and 26.6% CO$_2$
by mass ratio. The last fuel mixture was composed of 54% NG and 46% propane by mass ratio.

Table 3-2: Heating Value of Fuels

<table>
<thead>
<tr>
<th>Fuel</th>
<th>HHV, BTU</th>
</tr>
</thead>
<tbody>
<tr>
<td>NG</td>
<td>1026</td>
</tr>
<tr>
<td>NG+CO₂</td>
<td>900</td>
</tr>
<tr>
<td>NG+ Propane</td>
<td>1400</td>
</tr>
</tbody>
</table>
Chapter 4 Combustion Analysis and Heat Transfer Model

Base Heat Release Model

The gross HRR was calculated using the well-known single zone zero-dimensional heat release model [48]. With the assumptions of a uniform pressure, uniform temperature and ideal gas, the HRR can be calculated using equation (7).

\[
\frac{dQ}{d\theta}_{\text{gross}} = \left(\frac{\gamma_1}{\gamma_1 - 1}\right) \cdot P \cdot \frac{dV}{d\theta} + \left(\frac{1}{\gamma_1 - 1}\right) \cdot V \cdot \frac{dp}{d\theta} \quad \text{Eq. (7)}
\]

\(\gamma_1\) is the specific heat ratio for method 1. By utilizing the log of pressure and volume, the specific heat ratio for exhaust and intake is determined. Evidently, this type of practice leads to a specific heat ratio, which includes the heat loss. However, it lacks accuracy for calculating the heat loss during combustion, since it approximates zones of the combustion process of an ICE.

\[
\frac{dQ}{d\theta}_{\text{ gross}} = \left(\frac{\gamma_2}{\gamma_2 - 1}\right) \cdot P \cdot \frac{dV}{dt} + \left(\frac{1}{\gamma_2 - 1}\right) \cdot V \cdot \frac{dp}{dt} + \frac{dQ}{d\theta}_{\text{heat transfer}} \quad \text{Eq. (8)}
\]

\(\gamma_2\) is the specific heat ratio calculated for method 2. In the industry, the specific heat ratio is calculated from the net heat release equation in Heywood without the heat transfer term [48]. In contrast, the specific heat ratio in method 2 is implemented for calculating the gross heat release based on the composition and temperature of the bulk mixture. Then, it is evaluated using the ideal gas equation with the in-cylinder pressure and volume at the intake valve closing as a reference condition. Therefore, it contains the additional heat transfer term as shown in equation (8).

In this research, the specific ratio \(\gamma\) of the bulk mixture was calculated by examining the specific heat under constant volume equation (9):
\[
\bar{c}_{v,mix} = \sum X_i \cdot \bar{c}_{v,i} \quad \text{Eq. (9)}
\]

Where: \( X_i \) is the molar fraction; \( c_{v,i} \) is the specific heat ratio under constant volume calculated utilizing the equation:

\[
\text{(Specific Heat Value)} C_p^o = A + B \cdot T + C \cdot T^2 + D \cdot T^3 + \frac{E}{T^2} \quad \text{Eq. (10)}
\]

\[
\text{(Standard Enthalpy)} H^o - H^o_{298.15} = A \cdot T + \frac{B}{2} \cdot T^2 + \frac{C}{3} \cdot T^3 + \frac{D}{4} \cdot T^4 - \frac{E}{T} + F - H \quad \text{Eq. (11)}
\]

\( T \): temperature of the mixture

The constants for the calculation of the specific heat under constant can be found in the appendix. This data was derived from the calculating the trend line utilizing the data on specific heat for each of the selected species based on the data provided by National Institute of Standards and Technology (NIST).

**Estimation of Bulk Gas Temperature at Intake Valve Closing**

The bulk gas temperature was estimated from calculating the residual and fresh mass intake at intake valve closing. This was achieved by calculating the mass per cycle for the fuel and air.

\[
m_{\text{intake}} = \frac{m_{\text{fuel 1}}}{0.5 \cdot n_{\text{cylinders}}} \left( \frac{\text{kg}}{\text{cycle}} \right) \quad \text{Eq. (12)}
\]

The total fresh mass was calculated per cycle.

\[
m_{\text{fresh}} = m_{\text{air}} + \sum_{n=1}^{\infty} m_{\text{fuel 1,2,..n}} + \sum_{n=1}^{\infty} m_{\text{intake addition 1,2,..n}} \left( \frac{\text{kg}}{\text{cycle}} \right) \quad \text{Eq. (13)}
\]

The residual mass per cycle was calculated from ideal gas equation utilizing the pressure at bottom dead center and minimum volume based on the initial data.
\[ m_{\text{residual}} = \frac{P_{\text{BDC}} \cdot V_{\text{IVC}}}{R_{\text{mixture}} \cdot T_{\text{exhaust}} \cdot n_{\text{cylinders}}} \quad \text{(kg per cycle)} \quad \text{Eq. (14)} \]

Then, the cycle interval time was determined from the RPM data and crank angle data. Utilizing the mass flow rate equilibrium, the initial temperature was calculated.

\[ T_{\text{initial}} = T_{g} + \frac{(m_{\text{residual}}/m_{\text{fresh}}) \cdot (T_{\text{exhaust}} + 273.15)}{1 + (m_{\text{residual}}/m_{\text{fresh}})} \quad \text{(K)} \quad \text{Eq. (15)} \]

**Calculation of Bulk Mixture Temperature and Pressure**

The intake mass was calculated from ideal gas equation. The percentage mass fraction was calculated for each of the species for each fuel mixture.

\[ \% \text{MF}_{\text{fresh}} = (1 - \text{MFB}) \cdot m_{\text{initial,species}} \cdot m_{\text{fresh,species}} / M_{\text{species}} \quad \text{Eq. (16)} \]

\[ \% \text{MF}_{\text{residual}} = m_{\text{final,species}} \cdot m_{\text{residual,species}} / M_{\text{species}} \quad \text{Eq. (17)} \]

\[ \% \text{MF}_{\text{final}} = \text{MFB} \cdot m_{\text{final,species}} \cdot m_{\text{fresh,species}} / M_{\text{species}} \quad \text{Eq. (18)} \]

The enthalpy was calculated for each species.

\[ \sum H_r = x_{\text{initial,species}} \cdot [(h^o)_i + \Delta h_{\text{initial,species}}] \quad \text{Eq. (19)} \]

Utilizing the gas Shomate equations, the specific heat under constant volume were calculated.

\[ C_{v,\text{Burn,Residual,Fresh}} = \sum \% \text{MF}_{\text{Burn,Residual,Fresh}} \cdot C_{v,\text{Species}} \left(\frac{\text{kJ}}{\text{kmol} \cdot \text{K}}\right) \quad \text{Eq. (20)} \]

Furthermore, the gas constant for each of the specific gas species were calculated. Then, the specific heat ratio was calculated utilizing:

\[ \gamma_2 = \frac{c_p}{c_p - R_u} \quad \text{Eq. (21)} \]
Then, the specific heat ratio calculated in equation (21) is applied to equation (8) to calculated the gross heat release rate.

**Calculation of Heat Loss**

The heat transfer coefficient was determined by the Woschni equation:

\[
h = \alpha \cdot D^{m-1} \cdot T_g^{0.75-1.62m} \cdot p^m \cdot \left[ C_1 \cdot V_p + C_2 \cdot \frac{V_d \cdot T_r}{P_r \cdot V_r} (p - p_0) \right]^m \quad \text{Eq. (22)}
\]

\[m = 0.8 \quad \text{(standard value for SI engine)}\]

\(\alpha\) is the scaling factor that is iterated to a value to accurately calculate the heat transfer coefficient. Then, the heat transfer coefficient is applied to calculate the heat loss as demonstrated in many other experiments [50].

\[
\Delta Q_{\text{loss}} = h \cdot A \cdot (T_g - T_W) \cdot \Delta t \quad \text{Eq. (23)}
\]

The net heat release was calculated using the equation recommended by Heywood [48].

The gross heat release was calculated from the addition of the heat loss.

\[
\left[ \frac{dQ}{d\theta} \right]_{\text{gross}} = \left[ \frac{dQ}{d\theta} \right]_{\text{net}} + \left[ \frac{dQ}{d\theta} \right]_{\text{heat transfer}} \quad \text{Eq. (24)}
\]

The molecular weight was calculated at each step to maintain accuracy of the mixture and to re-calculate the specific gas constant at each step. Then, the temperature at the \(n^{\text{th}}\) step was determined from the ideal gas equation.

\[
T_n = \frac{\{[\Delta Q]_{\text{gross}} - \Delta W\}}{m_{\text{intake}} \cdot C_v \text{ of fuel+air}} + T_{n-1} \quad \text{Eq. (25)}
\]

This process was iterated to create the entire heat release and pressure curve. The iteration was designed to minimize percentage error between the cylinder pressure measured and heat release rate before and after combustion.
\[
P_{\text{calc}} = \frac{R_{\text{specific}} \cdot T_n \cdot m_{\text{intake}}}{\forall} \quad \text{Eq. (26)}
\]

The enthalpy balance was applied with low heating value of the fuel to determine the simulation results were within the limits of the theoretical maximum of the heat release curve.

\[
Q_{\text{in}} = Q_{\text{Gross}} = \sum H_p - \sum H_r = \eta_{\text{combustion}} \cdot m_f \cdot Q_{\text{LHV}} \quad \text{Eq. (27)}
\]

**Assumptions**

There are a few crucial assumptions for this model, which would lead to error between the actual measurements:

1) The combustion reaction burns completely based on the basic stoichiometric equations for each of the fuel mixtures. Lean and rich combustion is not taken into account throughout the process.

2) It is assumed there is no blowby, which would lead to higher error post-combustion for the calculations.

3) Assumes the temperature of the cylinder wall remains at 400 K, which will lead to error for the heat loss calculations.

4) The fuel mixtures in the cylinder acts as an ideal gas, which allows it to be approximated by the ideal gas equation.

5) Based on the Woschni equation, the intake, combustion and exhaust periods are set at specific crank angles. However, in a real engine, the values would differ based on which are the definitions utilized, which would have to be calibrated to maintain accuracy.
Comparison

Figure 4-1 shows the cylinder pressure of this engine operated with pure NG observed at spark timing (ST) 22.5 °CA BTDC. The peak cylinder pressure measured was 76.2 bar, which was observed at 13 °CA ATDC. This current pressure curve shown was the average of 200 engine operation cycles.

Currently, the industries utilize a simpler and less theoretical method to calculate the heat release of the fuel during combustion process, which will be referred to as method 1. It involves determining the polytropic gas constant during post-combustion and pre-combustion sections of the log pressure vs log volume graph from the engine pressure data. This gives two average specific values, one is utilized for the pre-combustion phase and the other one is utilized to calculate the post-combustion phase heat release. As shown in Figure 4-2, the post-combustion polytropic constant is 1.3163 and the polytropic compression process constant during the pre-combustion is 1.346. Applying the industry utilized method, the heat loss is assumed to be averaged throughout the periods, which generally leads to an underestimation.
Utilizing the Gas Shomate equation coefficients provided by the NIST, a more accurate specific heat ratio was calculated and applied to determining the heat release of the combustion process of this SI engine. This technique will be referred as method 2. As shown in Figure 4-3, the specific heat ratio drops from 1.28 to 1.20 as combustion occurs, but slowly recovers as the temperature drops. As demonstrated in Figure 4-4,
method 2 yields a significantly higher gross heat release rate than the industry’s log comparison method.

As illustrated in Figure 4-5 below, the combustion process calculated using Method 2 proceeds slightly faster than that calculated using Method 1 during early combustion stage but at a much slower rate during late combustion stage. Such a difference may be due to the increased heat loss calculated during late combustion stage. This is backed up by the heat release data, where it shows method 1 crossing the heat release curve of method 2 during the latter part of post-combustion phase.
Validation

There were two types of methods to validate the model. The first method utilized was pressure comparison. As demonstrated in Figure 4-6 below, both of the measure and calculated pressure data are in close proximity with each other.

The percentage error between the measured pressure data and the calculated pressure data observed during the pre-combustion compression process before spark timing (ST) ranges from 0.1-1.8%. Assuming the combustion occurs during spark timing and ends after the mass fraction burned achieves 100%, the error between the pressure measured and simulated during the combustion expansion process ranges from 0.98 – 1.41%. Assuming that the post-combustion phase involves the period after the Woschni equation assumed the exhaust period began, the difference between the measured pressure data and the calculated pressure data ranges about 2.13-2.84%.
Figure 4-6: Measured and Calculated Pressure Utilizing Woschni Heat Release Equation, Release Rate, Fuel: NG. ST: 22.5 °CA BTDC

Table 4-1: Percent Error between Calculated and Measured Pressure

<table>
<thead>
<tr>
<th>Spark Timing</th>
<th>-22.5</th>
<th>-20.5</th>
<th>-18.5</th>
<th>-22.5</th>
<th>-20.5</th>
<th>-18.5</th>
<th>-22.5</th>
<th>-20.5</th>
<th>-18.5</th>
</tr>
</thead>
<tbody>
<tr>
<td>#Run</td>
<td>1492</td>
<td>1493</td>
<td>1494</td>
<td>1500</td>
<td>1501</td>
<td>1502</td>
<td>1510</td>
<td>1511</td>
<td>1512</td>
</tr>
<tr>
<td>Type of Fuel</td>
<td>Natural Gas</td>
<td>Natural Gas + CO\textsubscript{2}</td>
<td>Natural Gas + Propane</td>
<td></td>
<td></td>
<td></td>
<td></td>
<td></td>
<td></td>
</tr>
<tr>
<td>Pre-Combustion Avg. Pressure Difference</td>
<td>1.56%</td>
<td>1.09%</td>
<td>1.59%</td>
<td>1.71%</td>
<td>1.16%</td>
<td>1.74%</td>
<td>0.19%</td>
<td>0.40%</td>
<td>1.14%</td>
</tr>
<tr>
<td>Combustion Avg. Pressure Difference</td>
<td>1.44%</td>
<td>1.40%</td>
<td>1.38%</td>
<td>1.40%</td>
<td>1.34%</td>
<td>1.34%</td>
<td>0.98%</td>
<td>0.97%</td>
<td>1.31%</td>
</tr>
<tr>
<td>Post-Combustion Avg. Pressure Difference</td>
<td>2.74%</td>
<td>2.84%</td>
<td>2.57%</td>
<td>2.54%</td>
<td>2.65%</td>
<td>2.37%</td>
<td>2.31%</td>
<td>2.13%</td>
<td>2.60%</td>
</tr>
</tbody>
</table>

This data is shown for all three fuel mixtures in Table 4-1, where the measured and calculated data is compared. From the table, it is evident that the combustion modelling utilizing method 2 is on average 1% more accurate for pre-combustion to combustion phase than post combustion phase. This is understandable because for post-combustion, since
the blowby is not accounted for in the pressure calculations, there will be higher deviation from the measured data. Comparing the different mixture of fuels, there does not seem to be a trend in the inaccuracy of the data.

Table 4-2: Heat Release Rate Validation

<table>
<thead>
<tr>
<th>Spark Timing</th>
<th>-22.5</th>
<th>-20.5</th>
<th>-18.5</th>
<th>-22.5</th>
<th>-20.5</th>
<th>-18.5</th>
<th>-22.5</th>
<th>-20.5</th>
<th>-18.5</th>
</tr>
</thead>
<tbody>
<tr>
<td>#Run</td>
<td>1492</td>
<td>1493</td>
<td>1494</td>
<td>1500</td>
<td>1501</td>
<td>1502</td>
<td>1510</td>
<td>1511</td>
<td>1512</td>
</tr>
<tr>
<td>Type of Fuel</td>
<td>Natural Gas</td>
<td>Natural Gas + CO₂</td>
<td>Natural Gas + Propane</td>
<td></td>
<td></td>
<td></td>
<td></td>
<td></td>
<td></td>
</tr>
<tr>
<td>Pre-Combustion HRR (kJ)</td>
<td>0.002</td>
<td>0.002</td>
<td>0.002</td>
<td>0.002</td>
<td>0.002</td>
<td>0.002</td>
<td>0.001</td>
<td>0.002</td>
<td>0.002</td>
</tr>
<tr>
<td>Post-Combustion HRR (kJ)</td>
<td>-0.018</td>
<td>-0.018</td>
<td>-0.018</td>
<td>-0.018</td>
<td>-0.018</td>
<td>-0.018</td>
<td>-0.009</td>
<td>-0.018</td>
<td>-0.018</td>
</tr>
</tbody>
</table>

The second type of method utilized was by iterating to verify that the heat release rate before and after combustion should be zero. Then, the scaling factor of the Woschni equation was iterated by increments of 0.01 to determine the lowest value approaching to 0 kJ from the calculated heat released during pre and post combustion. This data is shown in the Table 4-2 below. As demonstrated, the calculated gross heat release was less than the theoretical maximum, which demonstrated that the results were valid. From the comparison shown in Table 4-3, it is evident that method 2, which utilizes a temperature derived specific heat ratio yields a significantly higher net HRR.

Table 4-3: Net HRR Comparison

<table>
<thead>
<tr>
<th>Spark Timing</th>
<th>-22.5</th>
<th>-20.5</th>
<th>-18.5</th>
<th>-22.5</th>
<th>-20.5</th>
<th>-18.5</th>
<th>-22.5</th>
<th>-20.5</th>
<th>-18.5</th>
</tr>
</thead>
<tbody>
<tr>
<td>#Run</td>
<td>1492</td>
<td>1493</td>
<td>1494</td>
<td>1500</td>
<td>1501</td>
<td>1502</td>
<td>1510</td>
<td>1511</td>
<td>1512</td>
</tr>
<tr>
<td>Type of Fuel</td>
<td>Natural Gas</td>
<td>Natural Gas + CO₂</td>
<td>Natural Gas + Propane</td>
<td></td>
<td></td>
<td></td>
<td></td>
<td></td>
<td></td>
</tr>
<tr>
<td>Net HRR Method 2 (kJ)</td>
<td>5.679</td>
<td>5.746</td>
<td>5.806</td>
<td>5.764</td>
<td>5.862</td>
<td>5.940</td>
<td>5.711</td>
<td>5.701</td>
<td>5.786</td>
</tr>
</tbody>
</table>
As illustrated in the Table 4-4 below, there is a slight trend of a lower heating value resulting in a lower scaling factor. The scaling factor for the NG and propane mixture were the lowest.

The scaling factor for NG remained the highest throughout the entire test.

Table 4-4: Calculated Woschni Coefficients for Fuels

<table>
<thead>
<tr>
<th>Fuel</th>
<th>Natural Gas</th>
<th>Natural Gas + CO₂</th>
<th>Natural Gas + Propane</th>
</tr>
</thead>
<tbody>
<tr>
<td>Woschni Scaling Factor</td>
<td>0.34</td>
<td>0.33</td>
<td>0.32</td>
</tr>
</tbody>
</table>
Chapter 5 Combustion Process of SI Turbo Natural Gas Engine

This chapter examines the effect of fuel composition and spark timing on the combustion process and exhaust emissions. The heat release rate was calculated using Method 2. The heat loss was calculated using the revised Woschni equation with the scaling factor derived in Chapter 4. The heat release rate was further processed to derive the variation of the mass fraction burned with changes in crank angle, and a set of combustion parameters such as CA5, CA10, CA50, CA90, and CA95 representing the crank angle location at which the corresponding percentage of combustion energy has been released.

As shown in Figure 5-1, advancing the spark timing increased the peak cylinder pressure if it is earlier from BTDC. The peak pressure observed at spark timing 22.5 °CA BTDC was 78.54 bar while at 18.5 °CA BTDC was 72.07 bar. This represented almost a 9% decrease in peak cylinder pressure due to a difference of only four crank angle. This is the same for the heat release rate as shown in figure 5-2 below. The peak heat release rate at ST of 22.5 °CA BTDC was 0.3874 kJ/°CA while at 18.5 °CA BTDC was 0.3674 kJ/°CA. This

Figure 5-1: The effect of spark timing on cylinder pressure. Fuel: NG
represented a 5.5% decrease in peak gross heat release rate due to a difference of only four crank angle.

Figure 5-2: The effect of spark timing on gross heat release. Fuel: NG

Figure 5-3: The effect of spark timing on mass fraction burned. Fuel: NG
As demonstrated in Figure 5-3, advancing spark timing leads to a delayed mass fraction burned. This is emphasized in Table 5-1, where it is evident that as the spark timing is set closer to TDC, the ignition delay is increased and the combustion duration is increased. Therefore, although there was not as significant difference compared to the pressure data, it is noticeable, which emphasizes the importance of the spark timing for combustion analysis.

Table 5-1: Spark Timing Impact on Combustion Phasing, Fuel: NG

<table>
<thead>
<tr>
<th>Type of Fuel</th>
<th>Natural Gas</th>
</tr>
</thead>
<tbody>
<tr>
<td>Spark Timing</td>
<td>-22.5 -20.5 -18.5</td>
</tr>
<tr>
<td>CA5</td>
<td>-7.74 -6.60 -5.14</td>
</tr>
<tr>
<td>CA10</td>
<td>-4.49 -3.24 -1.64</td>
</tr>
<tr>
<td>CA50</td>
<td>3.86 5.40 7.35</td>
</tr>
<tr>
<td>CA90</td>
<td>10.59 12.33 14.59</td>
</tr>
<tr>
<td>CA95</td>
<td>11.83 13.58 15.90</td>
</tr>
</tbody>
</table>

Figure 5-4 below compares the cylinder pressure of this engine operated at three fuels. Adding propane increased the peak cylinder pressure from 75.6 bar to 80.0 bar. The propane and NG mixture generated the highest peak cylinder pressure due to propane’s higher flame speed, which would speed up the combustion process. The addition of CO2 decreased the peak pressure by about 250 kPa. This is understandable, since the excess CO2 would be taking up some of the space of the intake air, which would hamper combustion and yield a lower heat release rate and peak pressure.
The three different fuel mixtures are compared in Figure 5-5. The peak heat release rate observed with NG + Propane mixture was 0.4141 kJ/°CA, which was 9.6% higher compared to 0.3778 kJ/°CA observed with NG as fuel. The peak heat release rate observed with the addition of CO₂ to NG was 0.3523kJ/°CA or 6.75% lower than NG due to decelerated flame propagation rate, and slightly retarded combustion phasing as shown in Figure 5-4. The fast flame propagation of NG and propane mixture as fuel was also supported by the mass fraction burned shown in Figure 5-7.
Utilizing method 2, the heat loss was calculated as shown in Figure 5-6 for all three fuel mixtures at ST of 20.5 °CA BTDC. The highest peak heat loss was from NG and propane, which was 0.0085 kJ/°CA. The lowest peak heat loss was from NG and CO2 0.0074 kJ/°CA. The peak heat loss for NG remains between the three mixtures at 0.0077 kJ/°CA. Furthermore, the heat loss calculated from the Woschni equation represents about 15% of the total heat released as shown in Table 5-2 below, which is in line with past research [49].

Table 5-2: Total Heat Loss

<table>
<thead>
<tr>
<th>Spark Timing</th>
<th>-22.5</th>
<th>-20.5</th>
<th>-18.5</th>
<th>-22.5</th>
<th>-20.5</th>
<th>-18.5</th>
<th>-22.5</th>
<th>-20.5</th>
<th>-18.5</th>
</tr>
</thead>
<tbody>
<tr>
<td>Type of Fuel</td>
<td>Natural Gas</td>
<td>Natural Gas + CO2</td>
<td>Natural Gas + Propane</td>
<td></td>
<td></td>
<td></td>
<td></td>
<td></td>
<td></td>
</tr>
<tr>
<td>Heat Loss (Method 2, kJ)</td>
<td>1.014</td>
<td>0.994</td>
<td>0.966</td>
<td>0.982</td>
<td>0.964</td>
<td>0.941</td>
<td>0.962</td>
<td>0.952</td>
<td>0.951</td>
</tr>
</tbody>
</table>
Figure 5-6: The effect of fuel composition in heat loss. ST: 20.5 °CA BTDC

As shown in Table 5-3, there is significant fuel impact for combustion phasing. Utilizing the values from Table 5-3 to calculate the combustion parameters of combustion phasing. The ignition delay is defined as the difference between ST and CA5. The fast combustion duration is defined as the difference between CA90 and CA10. The combustion duration is the difference between CA95 and CA5.

Table 5-3: Fuel Impact On Combustion Phasing. ST: 20.5 °CA BTDC

<table>
<thead>
<tr>
<th>Fuel</th>
<th>CA5</th>
<th>CA10</th>
<th>CA50</th>
<th>CA90</th>
<th>CA95</th>
</tr>
</thead>
<tbody>
<tr>
<td>NG</td>
<td>-6.60</td>
<td>-3.24</td>
<td>5.40</td>
<td>12.33</td>
<td>13.58</td>
</tr>
<tr>
<td>NG+CO2</td>
<td>-6.23</td>
<td>-2.65</td>
<td>6.60</td>
<td>14.14</td>
<td>15.50</td>
</tr>
<tr>
<td>NG+Propane</td>
<td>-6.96</td>
<td>-3.88</td>
<td>4.01</td>
<td>9.68</td>
<td>10.39</td>
</tr>
</tbody>
</table>
Table 5-4: Fuel Composition Impact on Ignition Delay & Combustion Duration for Different Fuel Mixtures. ST: 20.5 °CA BTDC

<table>
<thead>
<tr>
<th>Fuel</th>
<th>Ignition delay, CA</th>
<th>Fast comb. Duration, CA</th>
<th>Comb. Duration, CA</th>
</tr>
</thead>
<tbody>
<tr>
<td>NG</td>
<td>13.90</td>
<td>15.58</td>
<td>20.18</td>
</tr>
<tr>
<td>NG + CO₂</td>
<td>14.27</td>
<td>16.79</td>
<td>21.72</td>
</tr>
<tr>
<td>NG + Propane</td>
<td>13.54</td>
<td>13.56</td>
<td>17.36</td>
</tr>
</tbody>
</table>

As shown in Table 5-4, the fuel mixture of NG and propane had the shortest ignition delay relative to the other fuels based on the same spark timing. From the gross heat release graph and the table given, the combustion ended significantly earlier than NG fuel by itself. As expected, the addition of CO₂ increased both the ignition delay and the combustion duration.

Figure 5-7: The effect of fuel composition in mass fraction burned. ST: -22.5° CA BTDC
As illustrated in Figure 5-7 propane has a significant initial mass fraction burn due to its high flame propagation. However, as all three mixtures approach 100%, the mass fraction progress narrows together. With CO₂ hampering the combustion process, it is expected that the NG and CO₂ mixture has the lowest mass fraction burn of all three fuels examined. The results obtained in this work also suggest that blending propane to low BTU gases may provide an effective approach of adjusting the heating value of available gaseous fuels for better combustion in SI gaseous fuel engines. The approach effectively utilizes the higher heating value and faster flame propagation rate of propane and high octane number of low BTU gases to further increase the brake thermal efficiency as higher compression ratio can be utilized. These concepts may also off-set the seasonal variation in the quality and quantity of low BTU gaseous produced in landfill and digester in wastewater treatment plants. Table 5-5 shows the engine-out emissions of CO₂, NOₓ, CO, CH₄, and UMHC.

Table 5-5: Engine Out Emissions. ST: 20.5 °CA BTDC. Unit: g/bhp-hr.

<table>
<thead>
<tr>
<th>Fuel</th>
<th>NG Only</th>
<th>NG + Propane</th>
<th>NG + CO₂</th>
</tr>
</thead>
<tbody>
<tr>
<td>CO₂</td>
<td>426.9</td>
<td>466.91</td>
<td>411.13*</td>
</tr>
<tr>
<td>NOₓ</td>
<td>11.75</td>
<td>13.01</td>
<td>12.79</td>
</tr>
<tr>
<td>CO</td>
<td>8.01</td>
<td>8.80</td>
<td>5.79</td>
</tr>
<tr>
<td>THC</td>
<td>0.52</td>
<td>0.47</td>
<td>0.51</td>
</tr>
<tr>
<td>NMHC</td>
<td>0.07</td>
<td>0.25</td>
<td>0.09</td>
</tr>
<tr>
<td>η_combustion</td>
<td>98.15 %</td>
<td>98.10%</td>
<td>98.8%</td>
</tr>
</tbody>
</table>

* CO₂ added to intake fuel was not accounted as exhaust emissions

NG yields the lowest NOₓ emissions, which is about 10% lower than other two fuels. The lowest CO₂ emissions were observed when operated at NG+CO₂. This is due to the best brake thermal efficiency observed with NG+CO₂ as shown in Table 5-4. In addition, the brake specific carbon monoxide emissions were 10 - 20% lower for the NG+CO₂ mixture.
The advantage of the propane and NG mixture is the THC emissions, which is 10 to 15\% lower than the THC emissions observed with other two fuel candidates. Nonetheless, all the brake specific emissions are before the after-treatment system, so therefore as long as the effectiveness of the after-treatment system is high enough, the engine will still be in compliance with the standards. The emissions of CO\(_2\), hydrocarbon, and CO were further processed to derive the combustion efficiency defined as the percentage of carbon in fuel converted to CO\(_2\). As shown in Table 5-6, the combustion efficiency calculated was 98.10\% to 98.8\% indicating the extent of complete combustion of gaseous fuel burned this engine.

Table 5-6: After-Treatment Out Exhaust Emissions. (g/bhp-hr) ST: 20.5 °CA BTDC

<table>
<thead>
<tr>
<th>Fuel</th>
<th>NG Only</th>
<th>NG + Propane</th>
<th>NG + CO(_2)</th>
</tr>
</thead>
<tbody>
<tr>
<td>CO</td>
<td>0.7031</td>
<td>0.6426</td>
<td>0.7573</td>
</tr>
<tr>
<td>NO(_x)</td>
<td>0.0504</td>
<td>0.0162</td>
<td>0.0594</td>
</tr>
<tr>
<td>NMHC</td>
<td>0.0034</td>
<td>0.0047</td>
<td>0.0040</td>
</tr>
<tr>
<td>THC</td>
<td>0.0252</td>
<td>0.0170</td>
<td>0.0125</td>
</tr>
</tbody>
</table>

Table 5-7: Exhaust Emissions and Regulations of EPA and CARB, g/bhp-hr

<table>
<thead>
<tr>
<th>Fuel</th>
<th>NO(_x)+NMHC</th>
<th>CO</th>
</tr>
</thead>
<tbody>
<tr>
<td>NG</td>
<td>0.0538</td>
<td>0.7031</td>
</tr>
<tr>
<td>NG+CO(_2)</td>
<td>0.0634</td>
<td>0.7573</td>
</tr>
<tr>
<td>NG+Propane</td>
<td>0.0209</td>
<td>0.6426</td>
</tr>
<tr>
<td>EPA Regulation</td>
<td>2.02</td>
<td>3.29</td>
</tr>
<tr>
<td>CARB Regulation*</td>
<td>0.75</td>
<td>3.28</td>
</tr>
</tbody>
</table>

*Voluntary

Table 5-7 compares if the emissions are in compliance with the current emission regulations applied by EPA and CARB. The emissions measured after the triple way catalyst were substantially lower than the emission regulations. Utilizing the most advanced TWC after-treatment system applied to the SI NG engines, the current emissions standards
is achievable on all three types of gaseous fuels. As shown in Table 5-6, for the current CO, THC, NO$_x$ and NMHC emissions, the engine is in compliance with both EPA and CARB regulations. The CO emissions are well below the 3.28 g/bhp-hr level [36]. The THC and NMHC emissions follow the same pattern. In addition, this engine operated on three fuels are also in compliance with California’s voluntary NO$_x$ + NMHC emissions levels [36]. This demonstrates that commercial application of the NG engine is feasible currently, as long as more research and development is completed.
Chapter 6 Small Engine Instrumentation

For continuing research on the heat transfer model, a small engine was modified for investigating exhaust emissions and combustion process analysis. The objective of the small engine research was to investigate the effect of fuel on the combustion and exhaust emissions from a small SI engine of the research on the heat transfer for small NG engines. The engine was a 3500 Watt Champion Model 46597 Gasoline Electric Generator photographed in the Figure 6-1 below.

![Figure 6-1: 3500W Champion Electric Generator](image)

It had a 196 cc single cylinder OHV engine. The generator contained a 3.8-gallon tank, which was capable of operating for 12 hours at 50% load. The pressure transducer that placed into the engine was a high temperature pressure sensor, Kistler 6056A.
However, due to the engine cylinder size, a sleeve was utilized for mounting the pressure sensor to insure a more stable and tighter fit as shown in Figure 6-2. The sleeve was designed utilizing a 3/8" bolt. A 4.4 mm drill bit was utilized for the entire length of the hole, while a 6.25 mm drill bit was utilized for the top section of the transducer sleeve. Afterwards, a 5.0 drill tap was utilized for the mid-section of the sleeve to produce the thread for the pressure transducer to lock in. This design provided a compact and secure fit for the pressure transducer.

![Figure 6-2: Pressure Transducer and Sleeve Modification](image)

The transducer sleeve was screwed into the engine cylinder. A regular bolt is currently screwed onto the placement for the pressure transducer sleeve in the Figure 6-3 below.
Figure 6-3: Pressure Transducer Sleeve Placement

The transducer sleeve ensured a stable pressure transducer and prevents the pressure transducer loosening throughout testing.

Due to the lack of a stable structure on the engine, the encoder was installed on metal brackets on the engine, which was then attached to the crankshaft using an extended metal thread as shown in Figure 6-4.

Figure 6-4: BEI H25 Incremental Encoder Mount Assembly
The crank angle measuring device utilized was a BEI H25 incremental optical encoder, which was accurate to the nearest 0.5 °CA. The NG and liquid propane conversion kit from Century Fuel Products as shown in Figure 6-5 was installed onto the engine for NG and liquid propane operation and testing. The process involved adding a metal adapter between the carburetor and air vent to attach the vapor hose to the regulator that was installed on the frame of the generator. Then a metal elbow was attached to a ball valve, which would be connected to the vapor hose installed with a high pressure regulator. The regulator would be attached to an adapter for connection directly with a gas tank.

![Figure 6-5: Century Link Tri-fuel Conversion Kit](image)

However, since the sleeve that was required in the NG conversion kit blocked an airflow hole in the carburetor, the NG conversion kit would have to be removed during gasoline operation, which is currently the reason that the metal adapter is de-attached from the current engine set-up. This engine has been instrumented for fuel impact on combustion process and heat release rate research.
Chapter 7 Conclusion

This research investigated the engine performance, combustion process, and exhaust emissions from a turbocharged SI WP-10 off-road engine developed to operate on gaseous fuels with a wide range of heating value (HHV range from 900 to 1400 BTU). A new method of calculating the specific heat ratio of the bulk gases was proposed and applied to calculate the heat release process. In addition, a scaling factor was proposed to increase the accuracy of the heat release calculations using Woschni equation. Based on the data presented in this research, the following conclusions can be drawn:

(1) The specific heat ratio calculated from temperature and bulk gas composition with the assumed complete combustion was lower than that derived from Log-P-Log V diagram, especially during the combustion phase. Therefore, heat release rate calculated utilization method 1 may not accurately reflect the actual heat release rate.

(2) The scaling factor of engine operated on NG at full load was 0.34. The scaling factor for fuel mixture of NG with CO₂ and NG with propane was 0.33, and 0.32, respectively. The scaling factor of this SI gaseous fuel engine in the range of 0.32 to 0.34 was significantly higher than the default scaling factor of 0.12793 for SI gasoline engine determined by Woschni.

(3) Based on the results, the addition of CO₂ will decrease the energy output with a 30% decrease in CO emissions and 5% decrease in CO₂ emissions. Meanwhile the addition of propane will increase peak heat release and decrease combustion duration indicating the accelerated combustion process.
This SI gaseous fuel engine equipped with TWC is in compliance with EPA and CARB emissions regulations. Therefore, it can be interpreted that natural gas engines could continue to remain regulatory complaint with a functioning TWC.

**Future Work**

The research results presented in this research also suggests that the blending of propane to low BTU gases such as digester gas and landfill gas will provide technical solution for the seasonal variation in low BTU gases quality and quantity. This practice can also be considered as a new approach of burning propane at high thermal efficiency. In addition, blending an array of gaseous fuels may yield better economic results.

For further research, more variation of NG engines will have to be tested. In the past, there have been a large amount of research for heavy duty and medium duty engines. However, there has been few research reports on small and compact engines, such as the portable electric gas generator. In addition, different combinations of fuel mixtures will be required to be tested to determine if different combinations of the fuels would be able to offset the few disadvantages of NG.
Bibliography


[29] Koebel, D., Supertruck Technologies for 55% Thermal Efficiency and 68%
Freight Efficiency, Directions in Engine Efficiency, Detroit, MI. 2012.


Appendix

Table A-1: Constant Values for Methane Shomate Equations

<table>
<thead>
<tr>
<th>Temperature (K)</th>
<th>298. - 1300.</th>
<th>1300. - 6000.</th>
</tr>
</thead>
<tbody>
<tr>
<td>A</td>
<td>-0.703029</td>
<td>85.81217</td>
</tr>
<tr>
<td>B</td>
<td>108.4773</td>
<td>11.26467</td>
</tr>
<tr>
<td>C</td>
<td>-42.52157</td>
<td>-2.114146</td>
</tr>
<tr>
<td>D</td>
<td>5.862788</td>
<td>0.13819</td>
</tr>
<tr>
<td>E</td>
<td>0.678565</td>
<td>-26.42221</td>
</tr>
<tr>
<td>F</td>
<td>-76.84376</td>
<td>-153.5327</td>
</tr>
<tr>
<td>G</td>
<td>158.7163</td>
<td>224.4143</td>
</tr>
<tr>
<td>H</td>
<td>-74.8731</td>
<td>-74.8731</td>
</tr>
</tbody>
</table>

Table A-2: Constant Value for Oxygen Shomate Equations

<table>
<thead>
<tr>
<th></th>
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<th></th>
</tr>
</thead>
<tbody>
<tr>
<td>A</td>
<td>31.32234</td>
<td>30.03235</td>
<td>20.91111</td>
</tr>
<tr>
<td>B</td>
<td>-20.23531</td>
<td>8.772972</td>
<td>10.72071</td>
</tr>
<tr>
<td>C</td>
<td>57.86644</td>
<td>-3.988133</td>
<td>-2.020498</td>
</tr>
<tr>
<td>D</td>
<td>-36.50624</td>
<td>0.788313</td>
<td>0.146449</td>
</tr>
<tr>
<td>E</td>
<td>-0.007374</td>
<td>-0.741599</td>
<td>9.245722</td>
</tr>
<tr>
<td>F</td>
<td>-8.903471</td>
<td>-11.32468</td>
<td>5.337651</td>
</tr>
<tr>
<td>G</td>
<td>246.7945</td>
<td>236.1663</td>
<td>237.6185</td>
</tr>
<tr>
<td>H</td>
<td>0</td>
<td>0</td>
<td>0</td>
</tr>
</tbody>
</table>

Table A-3: Constant Value for Nitrogen Shomate Equations

<table>
<thead>
<tr>
<th></th>
<th></th>
<th></th>
<th></th>
</tr>
</thead>
<tbody>
<tr>
<td>A</td>
<td>28.98641</td>
<td>19.50583</td>
<td>35.51872</td>
</tr>
<tr>
<td>B</td>
<td>1.853978</td>
<td>19.88705</td>
<td>1.128728</td>
</tr>
<tr>
<td>C</td>
<td>-9.647459</td>
<td>-8.598535</td>
<td>-0.196103</td>
</tr>
<tr>
<td>D</td>
<td>16.63537</td>
<td>1.369784</td>
<td>0.014662</td>
</tr>
<tr>
<td>E</td>
<td>0.000117</td>
<td>0.527601</td>
<td>-4.55376</td>
</tr>
<tr>
<td>F</td>
<td>-8.671914</td>
<td>-4.935202</td>
<td>-18.97091</td>
</tr>
<tr>
<td>G</td>
<td>226.4168</td>
<td>212.39</td>
<td>224.981</td>
</tr>
<tr>
<td>H</td>
<td>0</td>
<td>0</td>
<td>0</td>
</tr>
</tbody>
</table>
Table A-4: Constant Value for Carbon Dioxide Shomate Equations

<table>
<thead>
<tr>
<th>Temperature (K)</th>
<th>298. - 1200.</th>
<th>1200. - 6000.</th>
</tr>
</thead>
<tbody>
<tr>
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<td>24.99735</td>
<td>58.16639</td>
</tr>
<tr>
<td>B</td>
<td>55.18696</td>
<td>2.720074</td>
</tr>
<tr>
<td>C</td>
<td>-33.69137</td>
<td>-0.492289</td>
</tr>
<tr>
<td>D</td>
<td>7.948387</td>
<td>0.038844</td>
</tr>
<tr>
<td>E</td>
<td>-0.136638</td>
<td>-6.447293</td>
</tr>
<tr>
<td>F</td>
<td>-403.6075</td>
<td>-425.9186</td>
</tr>
<tr>
<td>G</td>
<td>228.2431</td>
<td>263.6125</td>
</tr>
<tr>
<td>H</td>
<td>-393.5224</td>
<td>-393.5224</td>
</tr>
</tbody>
</table>

Table A-5: Constant Value for Water(Gas) Shomate Equations

<table>
<thead>
<tr>
<th>Temperature (K)</th>
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<th>1700. - 6000.</th>
</tr>
</thead>
<tbody>
<tr>
<td>A</td>
<td>30.092</td>
<td>41.96426</td>
</tr>
<tr>
<td>B</td>
<td>6.832514</td>
<td>8.622053</td>
</tr>
<tr>
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